Convection Heat Transfer in Water-based Alumina Nanofluids

N.A. Roberts
Department of Mechanical Engineering
Vanderbilt University

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Introduction

Nanofluids are colloidal suspensions of nanoparticles in a base fluid

- Typical nanofluid properties
  - particles made of chemically stable metals, metal oxides or carbon in various forms
  - particles range in size between 1 and 100 nm
  - base fluid usually water and organic liquids

- Effects of nanofluids
  - greatly enhanced energy, momentum and mass transfer
  - reduced tendency for sedimentation and erosion of containing surfaces

- Applications of nanofluids
  - refrigeration
  - manufacturing
  - chemical and pharmaceutical processes
  - medical treatments
How do nanoparticles enhance thermal transport?

- suspended nanoparticles increase surface area and heat capacity of the fluid
- suspended nanoparticles increase the effective thermal conductivity of the fluid
- interaction and collision among particles, fluid and the flow passage surface are intensified
- mixing fluctuation and turbulence of the fluid are intensified
- dispersion of nanoparticles flattens the transverse temperature gradient of the fluid (changes the thermal boundary layer)
Experimental Setup: Convection Coefficient Measurement

Key measurements

- pressure drop along test section
- temperature profile along outside of test section (12 TC’s)
- inlet and outlet fluid temperatures
- heat dissipation from heater wire
- volumetric flow rate

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<th>Test section properties</th>
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<td>Tube</td>
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Nanoparticles and Preparation

- Nanoparticles (Al\textsubscript{2}O\textsubscript{3})
  - \(\gamma\) 10 nm
  - \(\gamma\) 20-30 nm

- Preparation
  - Nanoparticles are weighed and added to de-ionized water for different particle loadings
  - Nanoparticles are ultrasonicated for 1 hour to break up agglomerates

- Stability (from DLS)
  - \(\gamma\) 10 nm unstable in de-ionized water
  - \(\gamma\) 20-30 nm stable in de-ionized water
Results: Pressure and Temperature Drop/Increase

- Nearly equal pressure drop across the tube for all fluids
- Slight deviation from theoretical pressure drop for DI-water due to experimental setup

- Nearly equal temperature gain across the heated tube for the DI-water and the 0.5% nanofluid
- Greater temperature gain in the 1.5% nanofluid due to enhanced convective heat transfer
Results: Average Convection Heat Transfer Coefficients

heat transfer coefficient (W/m² K)

distance along pipe (x/l)

di-water
0.1% nanofluid
0.5% nanofluid
1.5% nanofluid
Results: Calculated Thermal Conductivity

The graph shows the thermal conductivity (W/m² K) as a function of volume loading (%). The data includes measurements for different volume loadings, indicating variability with the measured values. The graph also differentiates between two types of di-water, with distinct markers for each.
Conclusions/Future Work

- Observed enhancement in convection heat transfer coefficient in laminar flow regime
- Enhanced thermal conductivity with increasing volume loading
- No noticeable settling of nanoparticles or development of aggregates within hours
- Further investigation effects of nanoparticle size on heat transfer enhancement in water and ethylene glycol (want to find the limits of particle size, loading, etc.)
- Investigate nanofluids beyond laminar flow regime
- Compare nanofluids to base fluid in commercial and industrial systems
- Investigate long term properties/performance of nanofluids
- Develop model for enhancement in convection heat transfer coefficients and thermal conductivity